Depolarization of the hydrogen evolution reaction on cadmium electrodes in alkaline media

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Depolarization of the hydrogen evolution reaction on high purity polycrystalline cadmium electrodes in alkaline media ($12 \leq \text{pH} \leq 14$ and $5 \leq T \leq 55^\circ\text{C}$) produced by cathodization in the range of potential comprised between the $\text{Cd}/\text{Cd}(\text{OH})_2$ electrode potential and the net HER potential under solution stirring conditions has been studied. The depolarization effect depends on the perturbing potential programme and it is little affected by the alkaline cation in solution. Results are discussed in terms of three concurrent reactions, namely the electrochemical formation of $\text{Cd}(\text{OH})_2$ and soluble $\text{Cd}(\text{OH})_3^-$, the HER and the electrocrystallization of cadmium renewing the fresh active sites for the HER, SEM micrographs of activated cadmium electrodes reveal a heterogeneous surface topography of the new cadmium layers.

1. Introduction

The HER on cadmium in alkaline media has been investigated principally in relation to characterizing the negative cadmium electrode in a nickel–cadmium battery cell [1–3]. The overall reaction for hydrogen generation on cadmium in alkaline solutions is

The reversible potential of this reaction at pH 12 and 25°C is -0.713 V , a value which is only 7 mV more negative than the equilibrium potential of the reaction:

which is $E = -0.706\text{ V}$ [4]. This means that, theoretically, the cadmium electrode should generate some hydrogen when the nickel–cadmium cell operates open circuited and even more during the cell charging process as the potential of the cadmium electrode becomes more negative due to the relatively high overvoltage associated with that process.

It is generally accepted that the HER on cadmium in NaOH, KOH and CsOH solutions fits a $0.12\text{ V decade}^{-1}$ Tafel slope, the transfer coefficient being close to 0.5 [2, 3, 5]. Under steady-state conditions, the dependence of HER on pH suggests a slow direct discharge of water and the small variations in the current density/potential curves were attributed mainly to the different sizes of cations which affect the double layer.

The analysis of the transient electrochemical behaviour of freshly generated cadmium surfaces created by scratching shows that the maximum cathodic current density at fixed potentials under bare surface polarization is approximately independent of pH, although the bare surface mixed potential obeys a Nernst type relationship [6]. It should also be noted that kinetic measurements of HER on continuously renewed

cadmium surfaces in both neutral and sulphuric acid solutions exhibit an overpotential decrease by approximately 0.10–0.15 V with respect to results obtained at non-renewed surfaces, probably due to a lower effective activation energy for the HER [7, 8].

The cathodic currents on cadmium in 0.02–3.5 M KOH present a transition region which lies between the large current density increase according to high cathodic overpotentials and the fast cathodic current density decrease preceding the active metal dissolution range [9]. As the potential of zero charge, E_z , of cadmium is located, presumably, within this transition region, it was suggested that the cathodic current behaviour can be related to the change in the adsorbed $\text{H}_2\text{O}-\text{OH}^-$ ion layer on the cadmium surface. The competition between the oxide/hydroxide film formation and HER rates can result in a partially covered cadmium surface. It is significant to note that a similar but more pronounced cathodic transition region has been observed for zinc in slightly alkaline solutions [10]. Results obtained by using the rotating ring disc technique [11] demonstrated that a $\text{Cd}(\text{OH})_2$ film is already present on cadmium as the HER is taking place. Likewise, the reduction of the $\text{Cd}(\text{OH})_2$ film takes place, at least partially, through the dissolved cadmium species. On the other hand, it is well known that the physicochemical properties of different samples of $\text{Cd}(\text{OH})_2$ determine the rate of their chemical dissolution and the overpotential ratio for $\text{Cd}(\text{OH})_2$ electroreduction to HER [12]. The relative contribution of the HER varies strongly along the charging time.

Anodically formed oxide films on cadmium in 1–8 M NaOH are mainly reduced at cathodic overpotentials in the range of 0.02–0.1 V with respect to $\text{Cd}/\text{Cd}(\text{OH})_2$ [13], and at considerably higher overpotentials (approximately 0.3–0.5 V), the reduction of the remaining surface film takes place. The latter process appears to be strongly influenced by the HER. Otherwise, the charg-

ing plateau detected at high negative potentials in 0.1–7 M KOH solutions was assigned to the formation of either an intermetallic compound containing cadmium and potassium or a hydride [14]. These results illustrate the complexity of reactions which can occur on cadmium in the HER potential range in base solution and suggest the possibility of studying the mutual influence of the HER and $\text{Cd}/\text{Cd}(\text{OH})_2$ electrode reactions under preset perturbing potential conditions.

2. Experimental details

The experimental set up was described in previous publications [15, 16]. 'Specpure' cadmium (Johnson Matthey Chemicals Ltd) in the form of rotating discs (0.20 cm^2 apparent area) axially mounted in PTFE holders were used as working electrodes. The disc surface was polished successively with 400 and 600 grade emery papers, 1.0 and $0.3 \mu\text{m}$ grit alumina-acetone suspensions, thoroughly rinsed with triply distilled water and, finally, held for 5 min in the net HER region (-1.66 V to -1.56 V depending on solution pH) to attain a reproducible electroreduced initial metal surface.

The counterelectrode was a large area Pt sheet. Potentials were measured against an SCE reference electrode properly shielded and connected through a Luggin-Haber capillary tip, but in the text they are referred to the NHE scale.

Runs were made in $x \text{ M KOH}$ ($0.01 \leq x \leq 1$), 0.01 M LiOH and 0.01 M NaOH solutions in the $5\text{--}55^\circ \text{C}$ range under purified nitrogen gas saturation. The electrolyte solutions were prepared from analytical grade (p.a. Merck) chemicals and triply distilled water; the latter was previously boiled to remove CO_2 . The current density/applied potential (j/E) curves were recorded for electrodes either still ($\omega = 0$) or under rotation ($300 \leq \omega \leq 3000 \text{ r.p.m.}$) by employing the following perturbing potential programmes: (i) conventional single (STPS) or repetitive (RTPS) triangular potential sweeps between preset cathodic ($E_{s,c}$) and anodic ($E_{s,a}$) switching potentials at sweep rates (v) within the $0.0005 \leq v \leq 0.1 \text{ V s}^{-1}$ range; and (ii) combined either STPS or RTPS with intermediate potential holding at E_t for different times (τ). Electrochemical measurements were complemented with scanning electron microscopy using a Philips machine (505-B) with specimens previously subjected to triply distilled water and/or ethanol cleaning, drying and gold metallizing. Energy dispersive X-ray analysis of the electrode surfaces was carried out by using EDAX-PV 9100/60 equipment, and electron probe micro-analysis was performed employing a Microspec WDX-2A apparatus.

3. Results

The voltammogram of a cadmium electrode in stagnant 0.01 M KOH at $v = 0.1 \text{ V s}^{-1}$ between $E_{s,c} = -1.56 \text{ V}$ and $E_{s,a} = 0.24 \text{ V}$ shows two anodic peaks (I and II), a complex cathodic peak (III) and a net cathodic cur-

Fig. 1. Voltammogram (RTPS) run at $v = 0.1 \text{ V s}^{-1}$, $\omega = 0$, between $E_{s,c} = -1.56 \text{ V}$ and $E_{s,a} = 0.24 \text{ V}$ for $\text{Cd}/0.01 \text{ M KOH}$ (full trace). Potentiodynamic response after potential holding at different E_t for $\tau = 30 \text{ min}$, at $\omega = 2000 \text{ r.p.m.}$ (dashed traces). $E_t =$ (1) -0.96 V ; (2) -1.06 V ; (3) -1.16 V ; (4) -1.26 V ; (5) -1.36 V ; (6) -1.46 V .

rent at potentials lower than -1.1 V (Fig. 1). Peak I initiates at a potential very close to the equilibrium potential of the $\text{Cd}/\text{Cd}(\text{OH})_2$ electrode ($E = -0.706 \text{ V}$ at pH 12). Peak II is located at -0.25 V .

The voltammogram depicted in Fig. 1, particularly for peaks I, II and III changes little during potential cycling and it becomes practically independent of the solution stirring conditions. In addition, during a few initial cycles, under stirring, the cathodic current at $E < -1.1 \text{ V}$ can exceed that observed after prolonged cycling but these changes in the voltammogram are rather irreproducible unless a potential holding at E_t ($-1.42 \leq E_t \leq -0.96 \text{ V}$), is inserted into the potential scan, for $\tau = 30 \text{ min}$ at $\omega = 2000 \text{ r.p.m.}$ This combined potential sweep potential step treatment produces an appreciable increase in cathodic current at potentials lower than -1.2 V . This effect depends strongly on the E_t value (see dashed curves in Fig. 1), the maximum enhancement appearing for $E_t = -1.16 \text{ V}$. Under these conditions the cathodic current

Fig. 2. Dependence of current density at $E_{s,c} = -1.56 \text{ V}$ on E_t for different holding times τ obtained from the potential programme indicated in the figure for $\text{Cd}/0.01 \text{ M KOH}$. $v = 0.1 \text{ V s}^{-1}$. $\tau =$ (●) 3 min; (x) 10 min; (□) 30 min; (○) 60 min.

Fig. 3. Dependence of current density at $E_{s,c} = -1.56$ V on E_{τ} for a constant $\tau = 10$ min and $\omega_0 = 0$ (x) and $\omega_0 = 2000$ r.p.m. ($\square$) obtained from the potential programme shown in the figure for Cd/0.01 M KOH. $v = 0.1$ V s⁻¹.

measured from E_{τ} downwards greatly exceeds that recorded during the first cycles. Correspondingly, the cathodic current at $E_{s,c} = -1.56$ V resulting from the potential holding at E_{τ} for different times, τ , increases with τ (Fig. 2). The inclusion of the potential step at E_{τ} produces practically no voltammetric changes in the potential ranges of peaks I, II and III.

Similar results are obtained by using a single sweep potential programme depicted in Fig. 3 with $E_{s,a} = E_{\tau}$, although the magnitude of the cathodic current obtained at $E_{s,c} = -1.56$ V in the reverse scan appears to be slightly affected by ω_0 , the rotation speed of the working electrode and the initial positive going potential excursion. Furthermore, the value of ω set for the potential holding at $E_{\tau} = -1.16$ V determines the magnitude of the cathodic current at $E_{s,c}$ in the subsequent reverse scan (Fig. 4). At $E_{s,c} = -1.56$ V the cathodic current density increases linearly with the square root of ω , ω being the rotation speed of the working electrode during the potential step and subsequent reverse potential scan. The extrapolated value of j for $\omega \rightarrow 0$ equals 6.6 mA cm⁻², which is about 60% of the current density detected at $\omega = 3000$ r.p.m. However, at $\omega = 0$, for the potential holding at $E_{\tau} = -1.16$ V, practically no enhancement of the cathodic current at $E_{s,c} = -1.56$ V is observed under similar experimental conditions.

The cathodic current enhancement at $E_{s,c} = -1.56$ V remains even for those electrodes which have been removed from the electrolyte, rinsed with triply distilled water, dried, maintained at room atmosphere for 10 min and later re-immersed in the electrolyte to measure the current at $E_{s,c}$.

The increase in cathodic current resulting from the potential stepping at E_{τ} for the time τ , depends on

Fig. 4. Influence of ω on the voltammogram recorded after a potential holding at $E_{\tau} = -1.16$ V for $\tau = 10$ min from the potential programme depicted in the figure for Cd/0.01 M KOH. $v = 0.1$ V s⁻¹. $\omega =$ (1) 1000 r.p.m.; (2) 2000 r.p.m.; (3) 3000 r.p.m.

both E_{τ} and τ (Fig. 5). For E_{τ} values in the $-1.06 \leq E_{\tau} \leq -1.36$ V range the increase in cathodic current implies an induction time τ^* , which changes according to E_{τ} as shown in Fig. 5. It is clear that beyond τ^* the cathodic current at E_{τ} increases with a linear $\log j$ vs $\log t$ relationship whose slope is about 0.84 ± 0.08 . The minimum value of τ^* , which is about 3 min, results for $E_{\tau} = -1.16$ V. It should be noticed that for $E_{\tau} = E_{s,c} = -1.56$ V the cathodic current remains practically at the steady state value, at least for potential holding times of about 90 min.

Voltammetric runs carried out at $v = 0.0005$ V s⁻¹ between $E_{s,c} = -1.56$ V and different $E_{s,a}$ values, under stirring, show an ill-defined cathodic peak at approximately -1.26 V during the positive potential-going excursion (Fig. 6). In addition, during the reverse scan a considerable increase in cathodic current is noticed as $E_{s,a}$ exceeds the potential range of the new cathodic peak. But as $E_{s,a}$ is set within the poten-

Fig. 5. Dependence of the current density at different E_{τ} on the holding time from the potential programme indicated in the figure for Cd/0.01 M KOH. The variation of j before the potential holding is also included. $E_{\tau} =$ (■) -1.06 V; (Δ) -1.16 V; (x) -1.26 V; (○) -1.36 V; ($\square$) -1.46 V; (●) -1.56 V.

Fig. 6. Influence of E_{sa} on the voltammograms obtained at $v = 0.0005 \text{ V s}^{-1}$ and $\omega = 2000 \text{ r.p.m.}$ from $E_{sc} = -1.56 \text{ V}$ for Cd/0.01 M KOH.

tial range of the new cathodic peak, the reverse scan exhibits a small current hump at approximately -1.4 V , largely overlapping the cathodic current.

For the sake of comparison additional measurements were performed at pH 12 using LiOH, KOH and NaOH and in 1 M KOH. The strong influence of the perturbing potential programme on the cathodic current enhancement appears to be little affected by the nature of the cation. At pH 12 the cathodic current at $E_{sc} \approx -1.56 \text{ V}$, resulting from $E_t = -1.16 \text{ V}$, $\tau = 10 \text{ min}$ and $\omega = 1000 \text{ r.p.m.}$, in the $5\text{--}55^\circ \text{C}$ range fits an Arrhenius plot which is practically independent of the cation in solution. The apparent activation energy is $\Delta E^* \approx 33 \text{ kJ mol}^{-1}$ (Fig. 7).

Fig. 7. Arrhenius plot for the current density at $E_{sc} = -1.56 \text{ V}$ at different temperatures in the $5\text{--}55^\circ \text{C}$ range from the potential programme indicated in the figure for 0.01 M KOH (Δ), 0.01 M NaOH ($\square$) and 0.01 M LiOH ($\circ$). T is measured in K.

Fig. 8. Dependence of current density at $E_{sc} = -1.66 \text{ V}$ on E_t at different τ values from the potential programme shown in the figure for Cd/1 M KOH. $v = 0.1 \text{ V s}^{-1}$. $\tau = (\times) 10 \text{ min}$; ($\square$) 30 min; ($\circ$) 60 min.

Under comparable experimental conditions the cathodic current enhancement in 1 M KOH is considerably greater than in 0.01 M KOH, although in the former case results are less reproducible. The magnitude of the cathodic current at $E_{sc} = -1.66 \text{ V}$ after a potential holding at different E_t values for various times τ up to 60 min, shows that a large increase of j results for $-1.36 \leq E_t \leq -1.16 \text{ V}$, the maximum value of j being for $E_t = -1.16 \text{ V}$ at large τ (Fig. 8). It should be noticed that results shown in Fig. 2 also suggest a similar influence of E_t at large holding times for pH 12.

The current read at the hydrogen overpotential range (referred to the equilibrium potential of the hydrogen electrode in the solution) $0.4 \leq \eta_c \leq 0.7 \text{ V}$ in 1 M KOH from the voltammogram at $v = 0.1 \text{ V s}^{-1}$ for an activated electrode, at $E_t = -1.16 \text{ V}$ for $\tau = 60 \text{ min}$, exhibits an enhancement in the apparent cathodic current density of about 1.5 decades as compared to that obtained in 6 M KOH under steady state conditions at the same η_c range [2].

SEM micrographs of Cd electrodes in 0.01 M KOH, previously held at $E_t = -1.36 \text{ V}$, for $\tau = 180 \text{ min}$ (that is at the value of E_t at which the largest cathodic current enhancement is produced (Fig. 5)), show a clear heterogeneous change in surface topography consistent with the electrocrystallization of a Cd overlayer, which eliminates the typical pattern of the mechanically polished Cd surface (Fig. 9). Energy dispersive X-ray analysis and electron probe microanalysis indicate that Cd is the only component at the activated electrode surface.

4. Discussion

The HER activation effect for Cd in alkaline solutions can be summarized as follows.

(i) The effect is produced by holding the applied potential in a definite range going from the potential where the electroreduction of the oxide layer is apparently down to approximately -1.5 V .

(ii) For a constant potential holding time, the effect

Fig. 9. Scanning electron micrographs of a polished cadmium (a) and a cadmium specimen after potential holding at $E_t = -1.36$ V for $\tau = 180$ min in 0.01 M KOH (b). Scale 1 μ m.

becomes slightly more marked as ω increases; although stirring is essential to produce the effect its actual magnitude is not of a great importance as can be seen in Fig. 4. The small stirring effect can only be attributed to hydrogen bubble removal from the interface.

(iii) Independently of the value of τ at pH 12, there is a common optimal E_t value of -1.16 V for producing a maximum increase in cathodic current density at -1.56 V (Fig. 2).

(iv) The activation effect involves an induction period (τ^*), which goes through a minimum value for $E_t = -1.16$ V (Fig. 5). When the induction period is exceeded the kinetics of current increase fit a j vs t^n relationship for $E = E_t$, where n lies close to one.

(v) There is a well-defined potential range (-1.05 to -1.45 V) where the activation effect occurs (Figs 2 and 8). At potentials outside this critical region no effect on HER can be noticed.

(vi) SEMs of activated cadmium electrodes show considerable differences in the characteristics of the surface morphology. Energy dispersive X-ray analysis and electron-probe micro-analysis data confirm that the surface is exclusively cadmium.

(vii) The HER activation effect increases with the alkaline hydroxide concentration.

The explanation of these intriguing results must be consistent with the facts that no increase in the anodic

Table 1. Redox potentials of some reactions relevant for the present work

Reaction	E^0 (V)	E_{pH12} (V)
(1) $2H_2O + 2e^- \rightleftharpoons 2OH^- + H_2$	-0.831	-0.713
(2) $Cd(OH)_2 + 2e^- \rightleftharpoons Cd + 2OH^-$	-0.824 [4]	-0.706
(3) $Cd(OH)_3^- + 2e^- \rightleftharpoons Cd + 3OH^-$	-0.668 [4]	-0.668^*

* Calculated for $Cd(OH)_2$ saturation condition [22].

oxide layer formation charge is noticed for an activated electrode, that the apparent Arrhenius plots exhibit a slope which is practically independent of the degree of activation, and that the nature of the cation is, in principle, irrelevant (Fig. 7).

From the thermodynamic standpoint it is convenient to consider the equilibria involved in the potential range where the HER depolarization effect is noticed (Table 1). In addition, from data reported in the literature [17–19] for the value of the potential of zero charge, E_z for Cd in base solutions can be estimated as < -1.1 V. Hence, in the potential range where the depolarization effect is observed, one would expect that the Cd electrode surface is largely covered by OH^- ions, a situation which is assisted by the local increase in alkalinity resulting from the HER itself. Otherwise, according to the thermodynamics, in the potential range associated with the HER depolarization effect, the cadmium proper electrode reactions become feasible. Based on SEM micrographs the Cd surface consists of a heterogeneous surface involving anodic and cathodic patches analogous to a spontaneous corrosion process, which in turn influences the HER. This arises from electrodisolution and chemical dissolution of Cd as $Cd(OH)_2$ and $Cd(OH)_3^-$ at anodic surface sites and the electrodeposition of Cd at cathodic surface sites which continually renew the Cd surface, causing an overpotential decrease for the HER. Reactions involving Cd species are likely to involve equilibrium conditions, whereas the HER behaves as a clear irreversible reaction. In this sense, the effect could be similar to that reported for the renewed Cd surfaces in neutral and acid solutions [7, 8].

The influence of stirring on the depolarization effect can be explained in terms of H_2 bubble formation. This process implies a nucleation and growth of bubbles at a certain distance from the electrode surface. Local bubble formation acts against the depolarization effect. This is clearly noticed on increasing the applied cathodic potential where bubble formation destroys the quasi-steady situation reached for the formation of Cd species and its electrodeposition in the -1.1 to -1.4 V potential range where the activation of the HER is noticed. On the other hand, a similar situation arises even at lower potentials under no stirring due to the accumulation of bubbles. Therefore, the maximum depolarization effect of the HER results from a compromise between the potential applied to the electrode, where the above-mentioned concurrent reactions takes place, and the hydrodynamic conditions prevailing at the electrode surface which modify the

nucleation and growth process for H₂ bubble formation [20, 21].

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