

## Modeling of CO<sub>2</sub> storage in aquifers

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**Abstract.** Storage of CO<sub>2</sub> in geological formations is a means of mitigating the greenhouse effect. Saline aquifers are a good alternative as storage sites due to their large volume and their common occurrence in nature. The first commercial CO<sub>2</sub> injection project is that of the Sleipner field in the Utsira Sand aquifer (North Sea). Nevertheless, very little was known about the effectiveness of CO<sub>2</sub> sequestration over very long periods of time. In this way, numerical modeling of CO<sub>2</sub> injection and seismic monitoring is an important tool to understand the behavior of CO<sub>2</sub> after injection and to make long term predictions in order to prevent CO<sub>2</sub> leaks from the storage into the atmosphere. The description of CO<sub>2</sub> injection into subsurface formations requires an accurate fluid-flow model. To simulate the simultaneous flow of brine and CO<sub>2</sub> we apply the Black-Oil formulation for two phase flow in porous media, which uses the PVT data as a simplified thermodynamic model. Seismic monitoring is modeled using Biot's equations of motion describing wave propagation in fluid-saturated poroviscoelastic solids. Numerical examples of CO<sub>2</sub> injection and time-lapse seismics using data of the Utsira formation show the capability of this methodology to monitor the migration and dispersal of CO<sub>2</sub> after injection.

### 1. Introduction

Fossil-fuel combustion generates carbon dioxide (CO<sub>2</sub>), which is mainly discharged into the atmosphere, increasing its temperature (greenhouse effect). To minimize climate change impacts, geological sequestration of CO<sub>2</sub> is an immediate option [1]. Geologic sequestration involves injecting CO<sub>2</sub> into a target geologic formation at depths typically greater than 1000 m where pressure and temperature are above the critical point for CO<sub>2</sub> (31.6C, 7.38 MPa).

The CO<sub>2</sub> injection operation at the Sleipner gas field in the North Sea, operated by Statoil and the Sleipner partners, is the world first industrial scale CO<sub>2</sub> injection project designed specifically as a greenhouse gas mitigation measure [1]-[2]. CO<sub>2</sub> separated from natural gas produced at Sleipner is currently being injected into the Utsira Sand, a saline aquifer some 26000 km<sup>2</sup> in area. Injection started in 1996 and is planned to continue for about twenty years, at a rate of about one million tonnes per year.

Time-lapse seismic surveys aim to demonstrate storage integrity, provide early warning should any leakage occur and monitor the migration and dispersal of the CO<sub>2</sub> plume. Recent papers [3]-[4] successfully apply seismic modeling for monitoring the spatio-temporal distribution

of CO<sub>2</sub> using synthetic generated CO<sub>2</sub> saturation fields. Instead, in this work we employ numerical simulations of CO<sub>2</sub> injection; therefore saturation fields are obtained as a result of the simultaneous flow of CO<sub>2</sub> and brine in porous media.

The final objective is to test that underground storage is a safe and verifiable technology in the long term.

## 2. The Black-Oil formulation of two-phase flow in porous media

The simultaneous flow of brine and CO<sub>2</sub> is described by the well-known Black-Oil formulation applied to two-phase, two component fluid flow [5]. In this model, CO<sub>2</sub> may dissolve in the brine but the brine is not allowed to vaporize into the CO<sub>2</sub> phase. This formulation uses, as a simplified thermodynamic model, the following PVT data, determined using the Hassanzadeh's correlations [6]:  $R_s$ : CO<sub>2</sub> solubility in brine;  $B_{CO_2}$ : CO<sub>2</sub> formation volume factor, and  $B_b$ : brine formation volume factor. The nonlinear system of partial differential equation is,

$$\nabla \cdot \left( k \left( \frac{k_{rCO_2}}{B_{CO_2} \mu_{CO_2}} (\nabla p_{CO_2} - \rho_{CO_2} g \nabla D) + \frac{R_s k_{rb}}{B_b \mu_b} (\nabla p_b - \rho_b g \nabla D) \right) \right) + q_{CO_2} \quad (1)$$

$$= \frac{\partial \left[ \phi \left( \frac{S_{CO_2}}{B_{CO_2}} + \frac{R_s S_b}{B_b} \right) \right]}{\partial t},$$

$$\nabla \cdot \left( k \left( \frac{k_{rb}}{B_b \mu_b} (\nabla p_b - \rho_b g \nabla D) \right) \right) + q_b = \frac{\partial \left[ \phi \left( \frac{S_b}{B_b} \right) \right]}{\partial t}. \quad (2)$$

The unknowns are the fluid pressures  $p_{CO_2}, p_b$  and saturations  $S_{CO_2}, S_b$  for the CO<sub>2</sub> and brine phases. The parameters  $k$  and  $\phi$  are the absolute permeability and porosity respectively. Also, for  $\beta = CO_2, b$ , the functions  $k_{r\beta}, \mu_\beta$  and  $\rho_\beta$  are the relative permeability, viscosity, and density of the  $\beta$ -phase, respectively.

Two algebraic equations relating the saturations and pressures, complete the system:

$$S_b + S_{CO_2} = 1, \quad p_{CO_2} - p_b = P_C(S_b), \quad (3)$$

where  $P_C$  is the capillary pressure.

The solution of the Black-Oil fluid-flow model was obtained employing the public domain software BOAST [7], which solves the differential equations using IMPES, a semi-implicit finite difference technique [8].

## 3. Biot's Equations of Motion

Let us consider a 2D isotropic fluid-saturated porous material  $\Omega$ . The oscillatory motion of  $\Omega$  at the angular frequency  $\omega$  subject to external sources  $F^{(s)}$  and  $F^{(f)}$  obeys Biot's equation of motion [3]

$$-\omega^2 \rho_b u^{(s)} - \omega^2 \rho_f u^{(f)} - \nabla \cdot \sigma(u) = F^{(s)} \quad (4)$$

$$-\omega^2 \rho_f u^{(s)} - \omega^2 g u^{(f)} + i \omega b u^{(f)} + \nabla p_f(u) = F^{(f)}. \quad (5)$$

The unknowns are  $u^{(s)}$  and  $u^{(f)}$ , the time Fourier transforms (FT) of the averaged displacement vectors of the solid and fluid phases, respectively. Also,  $\rho_f$  and  $\rho_b$  denote the densities of the single-phase fluid and the bulk material,  $g$  and  $b$  are mass and viscous coupling coefficients,  $\sigma_{ij}$

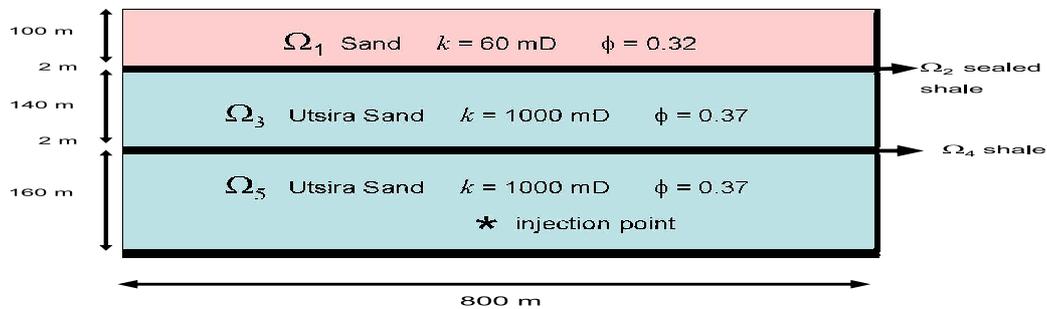
is the FT of the stress tensor of the bulk material and  $p_f$  is the FT of the fluid pressure. See [4] for the definition of the variables involved in (4)-(5).

Biot's equations were solved with the finite element method, employing a 2D non-conforming finite element space for each component of the solid displacement vector and the vector part of the Raviart Thomas Nedelec space of zero order for the fluid displacement [9].

#### 4. Numerical Experiments

##### 4.1. Idealized model of the Utsira formation

To test the proposed methodology, we consider an idealized geometrical and physical domain consisting of 5 regions as shown in Figure 1. The upper 100 m is region  $\Omega_1$ , a sand of permeability 60 mD and porosity 0.32.  $\Omega_2$  is a sealed shale 2 m thick, the top of the Utsira formation. Regions  $\Omega_3$  and  $\Omega_5$  are the Utsira formation, of permeability 1000 mD and porosity 0.37. We assume that  $\Omega_4$  is a sealed shale layer within the Utsira sand. The medium was excited with a compressional point source located at  $x=400$  m,  $z=710$  m.



**Figure 1.** Idealized model of the Utsira formation. The injection point is located at  $x=400$  m,  $z=1060$  m.

The Biot model assumes a single-phase fluid, therefore effective fluid density, viscosity and bulk modulus were obtained using the properties of the  $\text{CO}_2$  and brine weighted by the corresponding saturations computed by the fluid-flow simulator.

##### 4.2. Injection Modeling

Figure 2 shows the  $\text{CO}_2$  saturation distribution after 5 years of injection obtained by the BOAST simulator. A  $\text{CO}_2$  accumulation beneath the  $\Omega_4$  seal can be clearly observed.

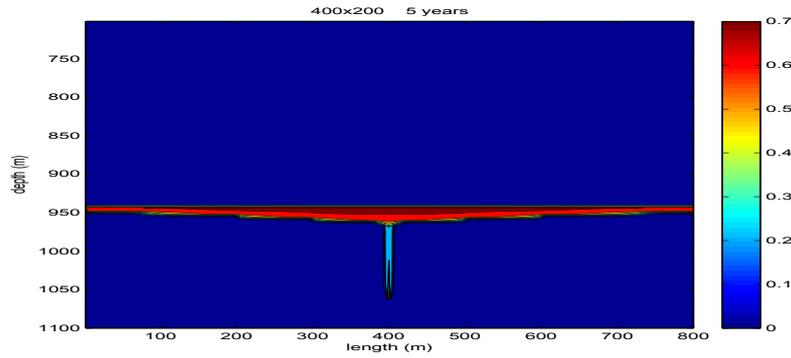
##### 4.3. Seismic Monitoring

Figure 3 displays traces of the vertical component of the particle velocity of the solid phase before (black curve) and after (red curve) 5 years of  $\text{CO}_2$  injection. The strong arrival at about 240 ms corresponds to a reflection due to the  $\text{CO}_2$  accumulation beneath the seal.

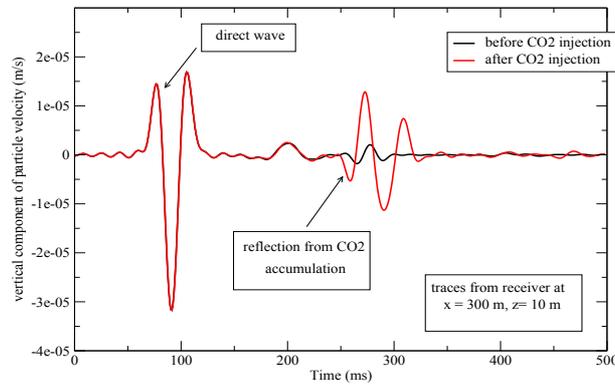
Time histories measured near the surface before (left plot) and after 5 years of  $\text{CO}_2$  injection (right plot) are shown in Figure 4.

The first reflection in both figures is due to the direct wave coming from the point source located at  $x=400$  m,  $z=710$  m. The second reflection in the time histories after 5 years, not observed before the injection, is generated by the  $\text{CO}_2$  accumulations below the thin shale layer at depth  $z=940$  m.

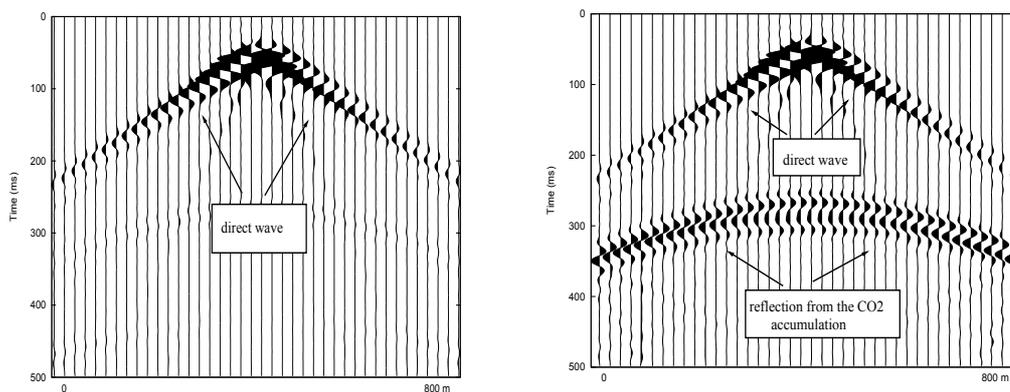
Figure 5 displays the vertical component of the solid phase velocity before and after 5 years of  $\text{CO}_2$  injection at 200 ms. At this time, the waves generated by the point source have generated



**Figure 2.** CO<sub>2</sub> saturation distribution after 5 years of injection. The injection point is located at x= 400 m, z= 1060 m.

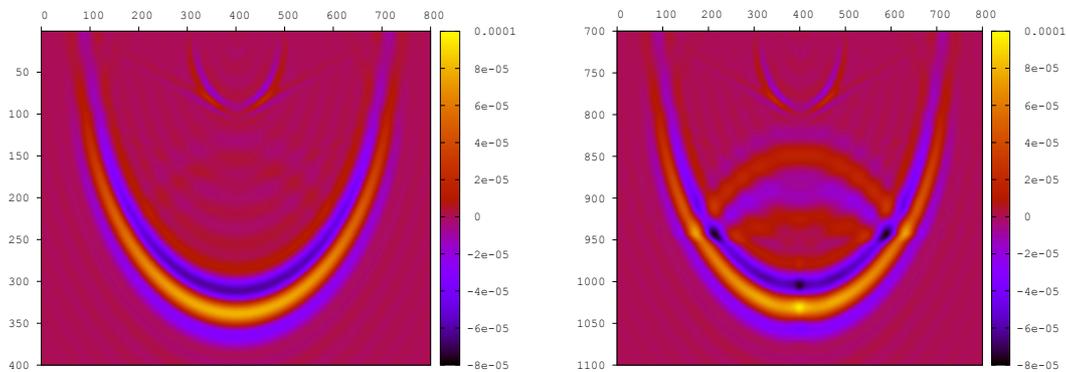


**Figure 3.** Traces of particle velocity of the solid phase before and after 5 years of CO<sub>2</sub> injection.



**Figure 4.** Time histories measured near the surface before and after 5 years of CO<sub>2</sub> injection.

reflected and transmitted waves due to the CO<sub>2</sub> accumulation below the thin shale layer at  $z = 940$  m.



**Figure 5.** Vertical component of the solid phase velocity at 200 ms before and after 5 years of CO<sub>2</sub> injection.

## 5. Conclusions

In this work we introduced a methodology to model and monitor CO<sub>2</sub> sequestration using numerical simulations. For that purpose we integrated numerical simulators of CO<sub>2</sub>-brine flow and seismic wave propagation. This methodology was tested with a numerical example showing the capability of seismic monitoring to identify the horizontal and vertical accumulations of CO<sub>2</sub>. Therefore, combining fluid-flow simulations with seismic methods constitute an important tool to analyze storage integrity, provide early warning should any leakage occur, and monitor the migration and dispersal of the CO<sub>2</sub> plume.

## 6. References

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