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Use of Agro-Industrial Wastes for the Production of a Wild Yeast Enzyme with Disintegration Activity on Plant Tissues

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HIGHLIGHTS

- Use of residues for the PGase production represented an economic and sustainable method.
- The activity of PGase enhanced 37 %, with respect to the value obtained with original medium.
- PGase of *W. anomalus* was able to disintegrate cassava tuber tissue and release the starch granules.

Abstract: The objective of the present study was to develop a cost-effective medium, using agro-industrial wastes for the production of a polygalacturonase by *Wickerhamomyces anomalus* of interest in cassava starch industries.

The effect of several raw agro-industrial wastes and others nutrients on polygalacturonase production by *W. anomalus*, were evaluated, in a reference fermentation medium, using statistical designs, by batch culture. The ability of the cell-free supernatant to extract cassava starch was evaluated.

Lemon peel was the best inducer for the production of PGase. Statistical analysis of the data showed that lemon peel, Mg⁺² and PO₄HK₂ had significant effect on PGase production, and the others variables (yeast extract, Ca⁺², Fe⁺², amino acid and trace element solution) were no significant. PGase synthesis reached ~31 EUmL⁻¹, in the OFM (glucose, lemon peel, urea, vitamins, KH₂PO₄ and MgSO₄), after 12 h of culture, at a lab scale

bioreactor. PGase of *W. anomalus*, was able to disintegrate cassava tuber tissue, and the starch granules contained within the cells were released into the reaction medium.

Lemon peel can be used as inducer for PGase production by *W. anomalus*, in a low cost culture medium, appropriate for the production of the enzyme at large scale.

Keywords: *Wickerhanomyces anomalous*; residues; Polygalacturonase; cassava starch extraction.

INTRODUCTION

The cost of the fermentation media is one of the determining factors in the production of enzymes. It is important to formulate a low cost culture medium and that it provide the nutritional requirements necessary for the proper growth of the microorganism [1-3]. Food and beverages industry generates, as a result of its activity, a large number of organic wastes as by-product of manufacturing processes. Consequently, the accumulation of great quantities of organic residues represents a risk to health and environment [4]. The production of microbial enzymes by a biotechnological process, using agricultural wastes in the culture medium, represents a suitable alternative for re-valorization of such a type of residues, reducing environmental pollution and generating products with high-added value, resulting in economic and ecological advantages [5-9].

Enzymes that disintegrate plant tissues are known as pectinolytic enzymes or pectinases. They constitute a group of enzymes that include polygalacturonase (PGase), pectin esterase (PE), and pectin lyase (PL) [10-12]. These enzymes are used in the processing of fruits and vegetables and are traditionally classified into two groups according to extent of disintegration. One group contains those enzymes that can totally disintegrate plant tissues. They are used mainly in production of foodstuffs with high proportions of soluble solids like tomato paste or puree, and also to improve yields in fruit juice production. The other group includes the macerating enzymes, which can produce a suspension of loose single cells and are used to prepare fruit nectar bases, vegetable purees, and baby and geriatric foods [13-16].

The conventional method for optimizing enzyme production by one variable at a time approach involves varying a single independent variable, while maintaining the others at a constant level. This one-dimensional approach is laborious and time-consuming. An alternative and more efficient approach is the use of statistical methods. The design of Plackett-Burman is a fractional factorial design, very useful for preliminary studies where a large number of variables must be investigated and in which the use of a complete factorial model becomes impractical due to the large number of required tests. Response surface methodology (RSM) involves full factorial search by examining simultaneous, systematic and efficient variation of all components [13,17-19].

In our previous studies on native microorganism from Misiones Province, we isolate a pectinolytic yeast strain (*Wickerhanomyces anomalus*) which produces an extracellular PGase with disintegrating activity on plant tissues [20]. Analysis of the culture supernatants revealed only a single enzyme activity, namely endo-PGase (EC 3.2.1.15). This enzyme was purified and characterized [21,22].

PGase of *W. anomalus*, was able to disintegrate crude cassava tuber tissue, and the starch granules contained within the cells were released into the reaction medium. In the conventional process, cassava starch is produced primarily by the wet milling of fresh cassava roots. A substantial amount of starch grains are damaged particularly during the rasping/pulping/grating processes. In addition, these mechanical steps are critical to the economy of the process due to the high energy consumption [23-25]. Therefore, the production of cassava starch including an enzymatic step seems to be an interesting alternative in order increase the quality of the starch obtained and also to reduce the energy consumption of the process.

The objective of this paper was the biotechnological valorization of agro-industrial wastes in order to design a cost-effective medium for the production of PGase by *W. anomalus*, considering its potential application in cassava starch industries.

MATERIAL AND METHODS

Yeast strain

W. anomalus, a yeast isolated from citrus fruit peels in the Province of Misiones, Argentina [20].

Culture media

Table 1 shows the composition of the Yeast medium (YM) used for the maintenance and propagation of *W. anomalus* and the composition of the Reference fermentation medium (RF medium) used for the production of the enzyme.

Table 1. Culture media.

Yeast medium (YM)	(gL ⁻¹)
Glucose (Britania, Buenos Aires, Argentina)	10
Yeast extract (Sigma Chemical Co., St. Louis, Mo, USA)	5
tryptone (Difco-Becton Dickinson & Co., Sparks, MD, USA)	5
Agar (Britania)	15
pH	5.1
Reference fermentation medium (RF medium) [26]	(gL ⁻¹)
Glucose (Britania)	10
Citrus pectin (Parafarm, Buenos Aires, Argentina)	5
Urea	1.4
KH ₂ PO ₄	1
MgSO ₄	0.5
CaCl ₂	0.1
FeCl ₃ ·6 H ₂ O	200 (µg ⁻¹)
vitamin solution	(1000 ×) 1 mL ⁻¹
amino acid solution	(100 ×) 10 mL ⁻¹
trace element solution	(1000 ×) 1 mL ⁻¹
pH	5.1
Vitamin solution (1000 ×) (Sigma) [27]	(µg ⁻¹)
D-biotin	2
calcium pantothenate	400
Pyridoxine	400
Thiamine	400
Amino acid solution (100 ×) (Sigma) [27]	(mgL ⁻¹)
Histidine	10
Methionine	20
Tryptophan	20
Trace element solution (1000 ×)	(µg ⁻¹)
CuSO ₄ ·5H ₂ O	40
MnSO ₄ ·H ₂ O	400
NaMoO ₄ ·2H ₂ O	200
ZnSO ₄ ·7H ₂ O	400

Distilled water was used for culture media preparation. All components of the medium were autoclaved (121 °C, 15 min), except in the case of vitamins and urea, which were sterilized separately by filtration through a cellulosic filter paper (0.22 µm, Sartorius).

Physicochemical characterization of agro-industrial residues

Agro-industrial residues (peels of orange, tangerine, lemon, banana, passion fruit, pineapple, papaya and grapefruit), were provided by local industries of Misiones Province, Argentina.

All residues were dried overnight at 45 °C in hot air drying oven (0.4 ms⁻¹), milled (propeller mill Arcano, 24000 rpm, 460W), passed through 35 mesh sieve to have uniform size particles of the material, and kept in air tight plastic containers for further analysis [28,29].

The agro industrial wastes were characterized by determining its centesimal composition. Carbohydrates, proteins, fats, dietary fiber, salts and ash content were determined using AOAC techniques [30]. Pectin was determined by measuring the amount of solubilized galacturonic acid (GA), by the m-hydroxy diphenyl method and was reported as mg of GA solubilized per mg of wet residue [31,32].

Batch cultures of *w. Anomalous*, in flasks

Enzyme production

Two hundred and fifty milliliter Erlenmeyer flasks with 45 mL of RF medium were inoculated with 5.0 mL of an appropriate dilution of a suspension of the microorganism ($OD_{620} = 0.96$), grown in YM medium (30°C, 24 h). The Erlenmeyer flasks were incubated at 30 °C, pH 5.1, for 16 h, on a rotary shaker incubator (MRC, TOU-50N, 25 mm shaking width) at 150 rpm [33]. The biomass was separated by centrifugation at $2.350 \times g$, at 5°C, for 10 min, washed carefully with sterile distilled water and used to inoculate subsequent fresh medium. Three precultures were performed. The fourth culture was centrifuged and the supernatant free of cells (enzymatic extract, EE) was frozen for further analytical assays [20].

Selection of a pectin-containing material as inductor for PGase production

Preliminary studies were carried out in order to select the best agro-industrial waste as inductor for PGase production by *W. anomalous*, using one variable at a time approach (OVAT) method. OVAT approach is based on changing one variable at a time without studying the interaction among the tested variables [34,35].

The strain was cultivated in the RF medium, containing 4% (wv-1) of each agro-industrial waste, instead of commercial citrus pectin. The fermentations were carried out as mentioned above, and experiment runs in the original culture medium (RF) were considered as control [6,8,36].

Experimental design and statistical analysis for culture medium optimization

Plackett-Burman design

The effect of different components in the RF medium containing the agro-industrial waste selected, instead of citrus pectin, for PGase production by *W. anomalous*, was evaluated. The mathematical method of Plackett-Burman (PB) screening design was used to evaluate the effect of eight independent variables. The variables studied were: agro-industrial waste, yeast extract, Ca^{+2} , Mg^{+2} , PO_4HK_2 , Fe^{+3} , amino acids and trace elements. Each independent variable was analyzed at two levels: high (+1) and low (-1) (Table 2). Based on the PB design, the corresponding matrix was obtained [8,35,37]. The fermentations were carried out as mentioned above and runs in the original RF medium, were considered as control.

Table 2. Factors, codes and real levels used in the Plackett-Burman design.

Variables	Code	Level of variables	
		(+1)	(-1)
Lemon peel waste (% wv ⁻¹)	A	10.00	2.00
Yeast extract (gL ⁻¹)	B	1.50	0.00
Ca ⁺² (gL ⁻¹)	C	0.10	0.05
Mg ⁺² (gL ⁻¹)	D	0.25	0.12
PO ₄ HK ₂ (gL ⁻¹)	E	0.50	0.25
Fe ⁺³ (gL ⁻¹)	F	0.0001	0.00
Amino acid solution	G	1.00	0.00
Trace element solution	H	1.00	0.00

Doehlert experimental design

The significant factors of the PB design were further optimized using response surface method (RSM) [38]. A design proposed by Doehlert was selected for studying the response surface [18, 19, 39]. The real values of the independent variables were coded based on a linear functionality between codified (Z) and actual values (X) according to:

$$X = Z \times \frac{\Delta X}{\Delta Z} + X_0 \quad (1)$$

Where X_0 is the real value of the central point and ΔX and ΔZ are the difference between the highest and lowest values of real and coded numbers, respectively.

For simplicity a full quadratic model containing six coefficients was used to describe the response observed.

$$Y = b_0 + \sum b_i x_i + \sum b_{ii} x_{ii}^2 + \sum b_{ij} x_j \quad (2)$$

Where Y is the response variable (PGase), b_0 a constant, and b_i , b_{ii} , and b_{ij} are the coefficients for the linear, quadratic and interaction effect, respectively. The number of experiments required in this design (N) is given by $N = n^2 + n + n_0$, where n is the number of variables and n_0 is the number of central points. Replicates at the central level of the variables were performed in order to have an estimation of the experimental variance.

Statistical analysis

All experiments were carried out in triplicate and their mean values were used. The statistical software Stat Graphics was used for analyzing the experimental data [40].

Validation of the experimental model

To validate the model, additional runs were carried out for PGase production in shake flasks containing the optimized fermentation (OF) medium, predicted by the RSM [3,41].

Bioreactor culture enzyme production

Batch fermentations were performed in a 5 L bioreactor (New Brunswick) containing 3 L of the optimized fermentation medium (OF), at 30 °C, with aeration (2.82 Lmin⁻¹) and agitation (500 rpm), during 16 h. Cultures were inoculated with an appropriate dilution of a suspension (in distilled water) of the microorganism, grown in Erlenmeyer flasks containing the same medium, at 30 °C, for 20 h. Samples (5 mL) were collected at suitable periods of incubation (1 h) on an ice bath and centrifuged. The EE, free of cells, were frozen for further analytical assays.

Application of the enzyme in cassava starch extraction

It was evaluated the potentiality of *W. anomalus* EE, to extract cassava starch. Cassava tubers (*Manihot esculenta* Crantz) were provided by a local industry of Misiones Province, Argentina. Tubers were washed under tap water, peeled and cut into sheets of approximately 1 cm thick. Sheets were weighed and subjected to enzymatic treatment. The reaction mixture was incubated at 40 °C, for 6 h, on a rotary shaker incubator (MRC, TOU-50N, 25 mm shaking width) at 150 rpm. After incubation time, the resultant suspensions were filtered through a double fold muslin cloth into a beaker and the filtrate was centrifuged at 2.350×g for 10 min. The supernatants were discarded and the sediment was washed twice with distilled water, dried at 45 °C for 24 h in hot air drying oven (0.4 ms⁻¹) (Oven Universal, JSGW, ambala cantt., India). The dried starch was weighed, ground using a laboratory mill and then passed through 100 mesh sieve and kept in air tight plastic containers for further analysis [42].

The yield starch was expressed as percentage of extracted material (EM) with respect to the dry weight of the original tissue (% ww-1) [43].

$$Yield(\% w/w) = EM^*(g) \times 100 / cassava (g) \quad (3)$$

In addition, it was evaluated, the starch extraction using a commercial pectinolytic enzyme (Novozym 33095, Frutos Patagónicos S.R.L., Argentina). The enzyme was diluted in order to obtain an extract enzymatic with a PGase activity similar to that of *W. anomalus* EE, and the starch extraction was carried out as mentioned above. Runs with distilled water instead of the enzymes, were considered as control. All experiments were carried out in triplicate and average values were taken for the calculations.

Analytical methods

Glucose: was determined using the glucose-peroxidase (Glicemia, Wiener, Argentina) method.

Polygalacturonase activity: was assayed by measuring the reducing groups released from 2 gL⁻¹ poligalacturonic acid (Sigma) solution, in sodium acetate/acetic acid buffer (0.2 M, pH 5.0) using Somogy-Nelson method. The reaction was carried out at 37 °C for 10 minutes. A calibration curve was made using galacturonic acid (GA) as standard. One unit of PGase was defined as the amount of enzyme that releases 1 µmol of GA per minute [26, 44-46].

RESULTS

Physicochemical characterization of agro-industrial residues

Table 3 shows the physicochemical determinations, on dry matter basis, of the agro-industrial residues.

Table 3. Physicochemical characterization of agro-industrial residues.

Mesh ⁽¹⁾	Papaya	Pineapple	Orange	Tangerine	Lemon	Banana	Passion fruit	Grapefruit
A	6.3±0.16	6.8±0.11	8.1±0.15	9.8±0.12	4.6±0.14	7.5±0.03	3.9±0.15	2.9±0.13
B	12.1±0.04	5.5±0.05	3.8±0.03	4.2±0.09	9.0±0.01	16.9±0.01	6.1±0.01	3.1±0.01
C	45.7±0.03	34.2±0.01	51.3±0.03	91.2±0.02	26.6±0.06	43.5±0.03	21.1±0.03	91.4±0.02
D	6.7±0.01	2.5±0.01	3.2±0.01	2.2±0.01	3.7±0.04	7.5±0.03	4.9±0.01	4.1±0.13
E	288.4±0.01	68.7±0.04	45.4±0.05	66.9±0.04	21.6±0.01	468.6±0.02	291.8±1.27	37.7±1.06
F	0.1±0.21	0.1±0.02	0.02±0.07	0.1±0.01	0.4±0.02	0.02±0.01	0.1±0.01	0.1±0.01
G	83.9±0.05	152.5±0.11	107.3±0.01	59.1±0.02	168.4±0.18	70.3±0.01	215.12±0.03	73.9±0.05
H	6.2±0.78	2.5±0.06	36.6±0.73	25.3±0.14	129.6±0.41	17.5±0.27	32.80±0.66	34.4±0.77
I	8.1±0.09	9.6±0.11	9.4±0.22	8.9±0.05	7.9±0.08	7.5±0.19	8.3±0.12	9.1±0.16

A: protein, B: Ashes, C: Carbohydrates, D: Fats, E: Sodium, F: Calcium, G: Dietary (o crude) fiber, H: Galacturonic acid (mg_{GA}/mg_{residue}), I: Water content, ⁽¹⁾ g % dry base.

The physicochemical analysis performed on different agro-industrial residues (Table 3) showed that the content of total protein was highest for tangerine peel (~9.87%), followed by orange peel (~8.12%) and lower for lemon peel (~4.56%). Grapefruit and tangerine wastes showed highest carbohydrates content with value of ~91.41% and ~91.20%, respectively.

The content of ash (minerals) was between 3.05 to 16.95 %, in the different residues evaluated.

Lemon peel presented the higher levels of calcium ~0.39% and pectin (determined as GA, ~129.57 mg_{GA}/mg_{residue}).

Batch cultures of *w. anomalus*, in flasks

Selection of a pectin-containing material as inductor for PGase production

Figure 1 shows the production of PGase by *W. anomalus* in the RF medium obtained at 16 h of culture, using different agro-industrial waste instead of commercial citrus pectin.

Enzyme activities are presented as percentage of that value attained with RF medium (30 °C, 16 h-180 rpm), which accounted for 100% (19.57 ± 0.55 EUmL⁻¹).

Lemon peel waste, was the best inducer for the production of PGase by *W. anomalus*, it was obtained a relative activity of 105.09% (21.74 EUmL⁻¹) when compared with that level obtained using RF medium.

PGase production was 16.52 ± 0.14 EUmL⁻¹ in the presence of orange, and this value has not significance difference (p<0.005) when it was used grapefruit, tangerine or passion fruit, as inductors. The used of papaya or banana, resulted in a lower production of the enzyme.

On the basis of these results, residue of lemon peels was selected as inductor for further experiments, in replacement of commercial citrus pectin and it contributes to the culture medium with other nutrients such as proteins, calcium and pectin.

Experimental design and statistical analysis for culture medium optimization

Plackett-Burman design

The matrix developed by the PB design, and the results (PGase activity) are presented in Table 4. The regression analysis is shown in Table 5 and in Figure 2 the Pareto chart.

Table 4. Plackett–Burman matrix (coded values) and PGase activity obtained.

Run order	Variable ^(a)								PGase ^(b) (UEmL ⁻¹)
	A	B	C	D	E	F	G	H	
1	1	-1	1	-1	-1	-1	1	1	6.89± 0.78
2	1	1	-1	1	-1	-1	-1	1	13.63± 0.48
3	-1	1	1	-1	1	-1	-1	-1	20.87± 1.40
4	1	-1	1	1	-1	1	-1	-1	20.56± 1.03
5	1	1	-1	1	1	-1	1	-1	21.46± 2.85
6	1	1	1	-1	1	1	-1	1	13.11± 2.14
7	-1	1	1	1	-1	1	1	-1	26.59± 1.26
8	-1	-1	1	1	1	-1	1	1	28.12± 1.12
9	-1	-1	-1	1	1	1	-1	1	28.80 2.31
10	1	-1	-1	-1	1	1	1	-1	21.82± 1.70
11	-1	1	-1	-1	-1	1	1	1	13.76± 1.76
12	-1	-1	-1	-1	-1	-1	-1	-1	11.64± 2.50

^(a)Mean of three values, SD within 10%. **A:** Lemon peel (%wv⁻¹); **B:** yeast extract (gL⁻¹); **C:** Ca⁺² (gL⁻¹); **D:** Mg⁺² (gL⁻¹); **E:** PO₄HK₂ (gL⁻¹); **F:** Fe⁺³ (gL⁻¹); **G:** amino acid solution; **H:** trace element solution. ^(b)Mean of three values, SD within 10 %.

Table 5. Analysis of variance (ANOVA) for the experimental parameters of PB design.

Variable	SS	DF	MS	F-value	p-value
A:Lemonpeelwaste	869.78	1	869.78	14.82	0.03*
B: yeast extract	590.66	1	590.66	1.01	0.39**
C: Ca ⁺²	20.99	1	20.99	0.36	0.59**
D: Mg ⁺²	217.25	1	217.25	37.01	0.01*
E:PO ₄ HK ₂	140.91	1	140.91	24.00	0.02*
F: Fe ⁺³	404.32	1	404.32	6.89	0.08**
G:amino acid solution	836.17	1	836.17	1.42	0.32**
H: trace element solution	288.76	1	288.76	4.92	0.11**
Error	176.10	3	587.01		
Corrected total	548.43	11			

* Significant values (p < 0.05); ** Non-significant values (p > 0.05); SM: Sum of squares; DF: degrees of freedom; MS: mean square. R²: 0.97.

Statistical analysis of the data (Table 5) showed that lemon peel, Mg⁺² and PO₄HK₂ had significant effect on PGase production (p < 0.05). The effect of the others variables (yeast extract, Ca⁺², Fe⁺², amino acids and trace

element solution) were no significant. The R² was 0.97, indicating that 97 % of the variability in the response could be explained by the model.

Pareto chart (Figure 2) indicates that Mg⁺² and PO₄HK₂ presented a positive effect in the range investigated. Lemon peel had a negative influence which means that, decreasing the concentration of this element in the culture medium, it will enhance the enzyme synthesis.

It is important to mention that when using lemon peel in the RF medium, instead of pectin, the influence of yeast extract, Ca⁺², Fe⁺², amino acid and trace element solution were not significant, this would be due to the fact that this agro-industrial residue is also a mineral, vitamins and protein sources, as it was determined in the characterization of the lemon peel (Table 5).

Subsequent studies were conducted using modified RF medium (RFM), according to the results of the PB design. The significant and positive factors (Mg⁺² and PO₄HK₂) were maintained at its high level. The others no significant variables (yeast extract, Fe⁺², Ca⁺², amino acid and trace element solution), were omitted and pectin was replaced by lemon peel.

Doehlert experimental design

A response surface method was employed to find the optimal level of the variables lemon peel and fermentation time, for the production of PGase by *W. anomalus*, using the RFM medium. The Doehlert experimental design was applied. The number of central points value (n₀) was fixed at 3 and with two factors, the total of points of Doehlert matrix was 9. Table 6 showed the matrix of the Doehlert design and the results of enzyme activity obtained in each experiment.

Table 6. Codified, actual values and PGase activity attained in the Doehlert design.

Exp.	Codified value		Actual value		PGase activity ^(a) (EUmL ⁻¹)
	Lemon peel waste	Fermentation time	Lemon peel waste (% pv ⁻¹)	Fermentation time (h)	
1	1	0	10	7.5	0.44± 0.16
2	0.50	-0.86	8	3	5.15±0.58
3	-0.50	-0.86	4	3	7.52± 0.34
4	-1	0	2	7.5	16.31±1.47
5	-0.50	0.86	4	12	25.51± 1.45
6	0.50	0.86	8	12	12.78± 1.27
7	0	0	6	7.50	11.21± 1.91
8	0	0	6	7.50	11.12±1.71
9	0	0	6	7.50	11.06± 1.61

^(a)Mean of three values, SD within 10%.

Regression coefficients were calculated in terms of coded values of independent variables and data were fitted to a second order polynomial equation (Equation 4).

$$\text{PGase} \left(\frac{\text{EU}}{\text{mL}} \right) = 11.13 - 7.81[\text{Lemon peel waste}] + 7.40[\text{Fermentation time}] - 2.75[\text{Lemon peel waste}]^2 - 5.98[\text{Lemon peel waste}][\text{Fermentation time}] + 3.06 [\text{Fermentation time}]^2 \quad (4)$$

The regression coefficient found (R²=0.99) indicated that the model was able to explain more than 99% of the observed response. Lemon peel and fermentation time showed both linear and quadratic effect significant (p < 0.05), as well as their interactions, on PGase production. The most important factor was lemon peel, with the highest coefficient, followed by fermentation time.

Figure 3 shows the response surface curve of PGase production by *W. anomalus* as function of the two independent variables.

The synthesis of the enzyme, increased when lemon peel concentration decreased from 10% (wv-1) to 2% (wv-1). As the fermentation time increased from 3 h to 12 h, a higher PGase production was observed.

The second order polynomial equation (eq. 4) determined a maximum PGase value of 30.06 ± 1.27 EUmL⁻¹, in the medium containing 2% (wv⁻¹) lemon peel at 12 h of culture, this value was higher to that obtained in RF medium.

The final composition of the Optimized Fermentation (OF) medium is shown in Table 7.

Table 7. Composition of the Optimized Fermentation Medium.

Component	
Glucose	10(gL ⁻¹)
Lemon peel waste	2% (wv ⁻¹)
Urea	1.4(gL ⁻¹)
KH ₂ PO ₄	0.5(gL ⁻¹)
Mg ⁺²	0.25(gL ⁻¹)
Vitamin solution	1000 ×

When estimating costs of the culture medium, it was obtained that the OF medium would cost US\$ 0.22L⁻¹, this value is lower than that for RF medium (US\$ 1.2L⁻¹).

Validation of the experimental model

The enzyme production attained in shake flasks, containing the culture medium described in Table 7 and with 2% of lemon peel was 31.12 ± 0.39 UEmL⁻¹, after 16 h of culture. Analysis of variance revealed no significant differences ($p < 0.05$) in PGase activity between predicted and experimental values, showing the validity of the model used.

Bioreactor culture enzyme production

The scaling-up effect on PGase production was evaluated in a 5 L bioreactor in the OF culture medium. Figure 4 shows the time course of a batch culture of *W. anomalus* in OF medium, at a laboratory scale bioreactor.

Figure 4 shows that the detectable production of PGase started at 2 h, obtaining a maximum production at 12 h, coinciding with glucose exhaustion. From this time, the enzymatic activity in the culture supernatant remained constant. It was obtained a maximum enzymatic production of 31.28 ± 0.93 EUmL⁻¹ at 12 h. The pH decreased slightly during the culture from an initial value of 5.1, up to about 4.9 at the end of the fermentation process.

Application of ee of *w. Anomalus* in cassava starch extraction

Figure 5 shows the material extracted (ME) from cassava tubers (*Manihot esculenta* Crantz), after centrifugation. The ME (starch, ashes, fibers, fats and proteins), with PGasa of *W. anomalus* resulted $44.5 \pm 0.98\%$ (gEM/gcassava dry). With the commercial enzyme, it was obtained a value of $40.14 \pm 0.48\%$ (gEM/gcassava dry). The control, in which the starch extraction was runs with distilled water instead of enzymes, was $6.38 \pm 0.76\%$.

DISCUSSION

Agro-industrial residues such as fruits peels are excellent substrates for bioprocesses in terms of its high content in carbohydrates, proteins, minerals salts, calcium, all essential nutrients for yeast grows. These materials, are natural source of pectic substances, and can be used as a substrate for the production of enzymes by microorganisms [47].

Larios and coauthors (1989) showed that endo-PGase production by *Aspergillus* sp. CH-Y-1043 was four times higher with lemon peel instead of pectin [48]. Maller and coauthors observed that orange peel was the best PGase inducer for submerged fermentation [49]. According to Embaby and coauthors, orange peel residues proved to be the best inducer for PGase production by *Bacillus licheniformis* SHG10 [35]. Similar results were obtained by Anuradha and coauthors, in the production of a PGase by *Aspergillus awamori* MTCC 9166 [37].

The effect of different nutrients on microbial enzyme production has been subject of different publications. Rekha and coauthors observed that orange peel and Mg⁺² had a great influence on PGase production by *T.*

frigidophilus profundus, whereas Fe^{+3} and Ca^{+2} showed less effect [50]. According to Ortiz and coauthors, an increase in K_2HPO_4 , traces solutions and Ca^{+2} factors exerts a positive effect on PGase production by *Aspergillus giganteus* NRRL10. Yeast extract, and Fe^{+2} had insignificant effect on enzyme productivity [51]. Poondla and coauthors studied the influence of different metal ions in the production of PGase by *Saccharomyces cerevisiae*, the production of enzymes increased considerably with $\text{MnSO}_4 > \text{KH}_2\text{PO}_4 > \text{ZnSO}_4 > \text{CaCl}_2 > \text{MgSO}_4 > \text{CoCl}_2$ [9].

In this paper, the decreased in PGase production observed when lemon peel concentrations increased, might be due to the increase in the viscosity of the culture medium, which caused problems to maintain the homogeneity and oxygen transfer problems during the fermentation process [12,52].

According to Naidu and Panda (1998) higher concentrations of carbon source inhibit enzyme synthesis [53]. Pedrolli and Carmona (2008) observed *A. giganteus* produced significant pectin lyase activity in medium with orange waste contents, with peak production at 2% (wv-1) [54]. According to Ahmed and Mostafa (2013), orange bagasse constitutes an excellent inducer substrate for PGase production by *P. pinophilum* Hedg NRRL 3503, which represented 69.20% increase in enzyme production compared with control [6]. Ahmed and coauthors showed maximum enzyme activity under optimum orange peel concentration of 4% for pectinase production by *A. niger* [55]. Nayyar and coauthors incorporated separately 1% of each agro-industrial wastes (apple peel, orange peel, lemon peel, potato peel and wheat bran) in a selected medium for PGase production by *Bacillus licheniformis* KIBE-IB3, further increase in concentration decline the PGase production [56].

Maidana and coauthors reported a maximum production of PGase by *W. anomalus* of $\sim 25.52 \text{ UEmL}^{-1}$ in a medium composed of (gL^{-1}): glucose, commercial citrus pectin, urea, yeast extract, KH_2PO_4 , CaCl_2 and MgSO_4 , in a batch system, at a lab scale bioreactor [19]. In this study it was obtained a highest production of the enzyme ($31.28 \pm 0.93 \text{ EUmL}^{-1}$), in an economical culture medium and using an agro-industrial waste.

In this paper was evaluated the potentiality of *W. anomalus* EE, to extract cassava starch. The EM extracted with PGasa of *W. anomalus* resulted $44.5 \pm 0.98\%$ (gEM/gcassava dry). Similar findings were reported for cassava starch extraction by Dzogbefia and coauthors using pectinase enzyme and by Sit and coauthors for taro starch extraction using cellulase and xylanase [57,58].

The optimization of the cassava starch extraction with *W. anomalus* PGase, the comparison and feasibility of costs with industrial processes, will be presented in a next work.

CONCLUSIONS

The production of PGase by *W. anomalus*, using agricultural wastes, such as lemon peel in the culture medium, represented a suitable alternative for re-valorization of such a type of residues.

The optimized fermentation medium included glucose, lemon peel, urea, vitamins, KH_2PO_4 and MgSO_4 . The activity of PGase was enhanced in almost 37 %, with respect to the value obtained with original Reference Fermentation medium.

PGase of *W. anomalus* was able to disintegrate completely cassava tuber tissue, and the starch granules contained within the cells were released into the reaction medium, resulting in a novel biotechnological method, alternative to the traditional one by mechanical means.

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